The listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- 1. (Cancelled)
- 2. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is a miniaturized miniaturised flow reactor.
- 3. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is a static micromixer.
- 4. (Currently Amended) Process according to Claim 1, characterized in that the A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor is connected to a capillary, preferably a heatable capillary, via an outlet, and reacting for a residence time, and isolating the resultant brominated organic compound from the reaction mixture.
- 5. (Currently Amended) Process according to Claim 1, characterized in that the volume of the microreactor is A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor with a volume of ≤ 10 μl, and reacting for a

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residence time, and isolating the resultant brominated organic compound from the reaction mixture preferably $\leq 1 \, \mu l$.

- 6. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is heatable.
- 7. (Currently Amended) Process according to Claim 1, characterized in that the microreactor A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor which has channels having a diameter of from 10 to 1000μm, and reacting for a residence time, and isolating the resultant brominated organic compound from the reaction mixture preferably from 20 to 800 μm, particularly preferably from 30 μm to 400 μm.
- 8. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the resultant reaction mixture flows through the microreactor at a flow rate of from 0.1 μm/min to 10 ml/min, preferably from 1 μl/min to 1 ml/min.
- 9. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the residence time of the resultant mixture compounds employed in the microreactor, where appropriate or in the microreactor and the capillaries, is ≤ 3 hours, preferably ≤ 1 hour.
- 10. (Currently Amended) Process according to Claim 1, characterised in that it A process according to claim 7, which is carried out at a temperature of from -90 to +150°C, preferably from -20 to +40°C, particularly preferably from -10 to +20°C.
- 11. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the course of the reaction is monitored by chromatography, preferably gas chromatography, and optionally where appropriate regulated.

- 12. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the brominated compound product is isolated from the reaction mixture by extraction or precipitation.
- 13. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the brominating reagent employed is elemental bromine, dibromoisocyanuric acid, N-bromosuccinimde, hypobromous acid, organic hypobromites, preferably trifluoroacetyl hypobromite, N-bromoacetamide, N bromophthalimide, pyridinium perbromide and/or dioxane dibromide.
- 14. (Currently Amended) Process according to Claim 1, characterised in that the A process according to claim 7, wherein a catalyst is present, which catalyst employed is iodine, a mineral acid acids, preferably sulphuric acid or nitric acid, and/or a Lewis acid acids, preferably aluminum halides, iron halides, zine halides or antimony halides.
- 15. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein between 0.1 and 100 mol% of, preferably between 1 and 10 mol%, of the catalyst is present are employed, based on the amount of organic compound employed.
 - 16. (Cancelled)
 - 17. (Cancelled)
 - 18. (Cancelled)
 - 19. (Cancelled)
- 20. (New) A process according to claim 4, wherein the capillary is heatable.

- 21. (New) A process according to claim 5, wherein the volume of the microreactor is $\leq 1 \, \mu l$.
- 22. (New) A process according to claim 7, wherein the channels have a diameter of 20 to $800\mu m$.
- 23. (New) A process according to claim 7, wherein the channels have a diameter of 30 to $400\mu m$.
- 24. (New) A process according to claim 7, wherein a catalyst is present, which catalyst is iodine, sulphuric acid, nitric acid, an aluminum halide, iron halide, zinc halide or antimony halide.
- 25. (New) A process according to claim 7, wherein the microreactor has a volume of \leq 10 μ l and/or is connected to a capillary via an outlet.